

The listing of claims will replace all prior versions, and listings, of claims in the application:

Listing of Claims:

1. (Cancelled)
2. (Currently Amended) Process according to Claim 1, characterised in that A process according to claim 7, wherein the microreactor is a miniaturized ~~miniaturised~~ flow reactor.
3. (Currently Amended) Process according to Claim 1, characterised in that A process according to claim 7, wherein the microreactor is a static micromixer.
4. (Currently Amended) Process according to Claim 1, characterized in that the A process for brominating an organic compound, comprising mixing an organic compound in liquid or dissolved form with a brominating reagent in liquid or dissolved form, optionally in the presence of a catalyst in liquid or dissolved form, in at least one microreactor is connected to a capillary, preferably a heatable capillary, via an outlet, and reacting for a residence time, and isolating the resultant brominated organic compound from the reaction mixture.
5. (Currently Amended) Process according to Claim 1, characterized in that the volume of the microreactor is A process for brominating an organic compound, comprising mixing an organic compound in liquid or dissolved form with a brominating reagent in liquid or dissolved form, optionally in the presence of a catalyst in liquid or dissolved form, in at least one microreactor with a volume of $\leq 10 \mu\text{l}$, and reacting for a

residence time, and isolating the resultant brominated organic compound from the reaction mixture preferably $\leq 1 \mu\text{l}$.

6. (Currently Amended) Process according to Claim 1, characterised in that A process according to claim 7, wherein the microreactor is heatable.

7. (Currently Amended) Process according to Claim 1, characterised in that the microreactor A process for brominating an organic compound, comprising mixing an organic compound in liquid or dissolved form with a brominating reagent in liquid or dissolved form, optionally in the presence of a catalyst in liquid or dissolved form, in at least one microreactor which has channels having a diameter of ~~from~~ 10 to 1000 μm , and reacting for a residence time, and isolating the resultant brominated organic compound from the reaction mixture preferably from 20 to 800 μm , particularly preferably from 30 μm to 400 μm .

8. (Currently Amended) Process according to Claim 1, characterised in that A process according to claim 7, wherein the resultant reaction mixture flows through the microreactor at a flow rate of ~~from~~ 0.1 $\mu\text{l}/\text{min}$ to 10 ml/min , ~~preferably from 1 $\mu\text{l}/\text{min}$ to 1 ml/min .~~

9. (Currently Amended) Process according to Claim 1, characterised in that A process according to claim 7, wherein the residence time of the resultant mixture compounds employed in the microreactor, ~~where appropriate~~ or in the microreactor and the capillaries, is ≤ 3 hours, ~~preferably ≤ 1 hour.~~

10. (Currently Amended) Process according to Claim 1, characterised in that it A process according to claim 7, which is carried out at a temperature of ~~from~~ -90 to +150°C, ~~preferably from -20 to +40°C, particularly preferably from -10 to +20°C.~~

11. (Currently Amended) Process according to Claim 1, characterised in that A process according to claim 7, wherein the course of the reaction is monitored by chromatography, ~~preferably gas chromatography, and optionally where appropriate~~ regulated.

12. (Currently Amended) Process according to Claim 1, characterised in that A process according to claim 7, wherein the brominated compound product is isolated from the reaction mixture by extraction or precipitation.

13. (Currently Amended) Process according to Claim 1, characterised in that A process according to claim 7, wherein the brominating reagent employed is elemental bromine, dibromoisocyanuric acid, N-bromosuccinimide, hypobromous acid, organic hypobromites, preferably trifluoroacetyl hypobromite, N-bromoacetamide, N – bromophthalimide, pyridinium perbromide and/or dioxane dibromide.

14. (Currently Amended) Process according to Claim 1, characterised in that the A process according to claim 7, wherein a catalyst is present, which catalyst employed is iodine, a mineral acid acids, preferably sulphuric acid or nitric acid, and/or a Lewis acid acids, preferably aluminum halides, iron halides, zinc halides or antimony halides.

15. (Currently Amended) Process according to Claim 1, characterised in that A process according to claim 7, wherein between 0.1 and 100 mol% of, preferably between 1 and 10 mol%, of the catalyst is present are employed, based on the amount of organic compound employed.

16. (Cancelled)

17. (Cancelled)

18. (Cancelled)

19. (Cancelled)

20. (New) A process according to claim 4, wherein the capillary is heatable.

21. (New) A process according to claim 5, wherein the volume of the microreactor is $\leq 1 \mu\text{l}$.
22. (New) A process according to claim 7, wherein the channels have a diameter of 20 to $800\mu\text{m}$.
23. (New) A process according to claim 7, wherein the channels have a diameter of 30 to $400\mu\text{m}$.
24. (New) A process according to claim 7, wherein a catalyst is present, which catalyst is iodine, sulphuric acid, nitric acid, an aluminum halide, iron halide, zinc halide or antimony halide.
25. (New) A process according to claim 7, wherein the microreactor has a volume of $\leq 10 \mu\text{l}$ and/or is connected to a capillary via an outlet.